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### AMENDMENTS TO THE CLAIMS

1. (Currently amended) A method for the preparation of halogenated benzonitriles by ~~vapour~~vapor phase ammoxidation of halogenated C<sub>1</sub> to C<sub>6</sub> alkyl benzenes, in the presence of water ~~vapour~~vapor, at a reaction temperature ~~comprised~~ in the range of 300 to 500 °C, using a three-component catalyst into a fixed bed reactor wherein said catalyst consists of a promoted VPO active phase provided on a carrier.
2. (Currently amended) A ~~The~~ method according to claim 1, wherein said reaction temperature is ~~comprised~~ in the range of 350 to 450 °C.
3. (Currently amended) A ~~The~~ method according to claim 1 ~~or 2~~, wherein the residence time of the halogenated C<sub>1</sub> to C<sub>6</sub> alkyl benzene in said reactor is less than 10 seconds, ~~preferably less than 8 seconds~~.
4. (Currently amended) A ~~The~~ method according to ~~any of claims 1 to 3~~ claim 1, wherein said halogenated C<sub>1</sub> to C<sub>6</sub> alkyl benzene is di- or tri-halogenated C<sub>1</sub> to C<sub>6</sub> alkyl benzene.
5. (Currently amended) A ~~The~~ method according to claim 4, wherein said di- or tri-halogenated C<sub>1</sub> to C<sub>6</sub> alkyl benzene is di-halogenated toluene.
6. (Currently amended) A ~~The~~ method according to claim 5, wherein said di-halogenated toluene is 2,6-dichlorotoluene.
7. (Currently amended) A ~~The~~ method according to ~~any of claims 1 to 6~~ claim 1, wherein said catalyst is provided on an Al<sub>2</sub>O<sub>3</sub> carrier.
8. (Currently amended) A ~~The~~ method according to ~~any of claims 1 to 6~~ claim 1, wherein said catalyst is provided on a TiO<sub>2</sub> carrier.
9. (Currently amended) A ~~The~~ method according to claim 8, wherein said TiO<sub>2</sub> carrier consists of the anatase phase.
10. (Currently amended) A ~~The~~ method according to ~~any of claims 1 to 9~~ claim 1, wherein said catalyst comprises a V<sub>1</sub>P<sub>a</sub>M<sub>b</sub>Al<sub>c</sub>O<sub>x</sub> or V<sub>1</sub>P<sub>a</sub>M<sub>b</sub>Ti<sub>c</sub>O<sub>x</sub> catalyst wherein M is ~~chosen~~ selected from the group ~~comprising~~ consisting of Cr, Fe, Co and Mo; a is 0.1 - 2.0; b is 0.002 - 1.0; c is 2.0 - 10.0, and x is determined by the valences of other component elements.
11. (Currently amended) A ~~The~~ method according to claim 10, wherein M is Co or Cr.

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12. (Currently amended) A ~~The~~ method according to ~~any of claims 1 to 11~~ claim 1, whereby the catalyst is diluted with an inert medium in the ratio of 0.5 to 2.0 by weight with respect to the weight of said catalyst prior to its addition to the reactor.

13. (Currently amended) A ~~The~~ method according to claim 12 wherein said inert medium comprises ~~corundum~~ corundum particles, porcelain beads, quartz beads, glass beads or the like.

14. (Currently amended) A ~~The~~ method according to ~~any of claims 1 to 13~~ claim 1, comprising the step of supplying a halogenated alkane to said reactor.

15. (Currently amended) A supported and promoted VPO catalyst, suitable for use in a method according to ~~any of claims 1 to 14~~ claim 1, obtainable by a process comprising the steps of:

- preparing a bulk VPO precursor;
- impregnating said bulk VPO precursor with a promoter element in order to obtain a bulk promoted VPO precursor; and
- adding a carrier to said bulk promoted VPO precursor,
- and calcining the resultant mixture under a weakly oxidising atmosphere of O<sub>2</sub>/N<sub>2</sub> to obtain a supported and promoted VPO catalyst,

whereby said catalyst is a V<sub>1</sub>P<sub>a</sub>M<sub>b</sub>Al<sub>c</sub>O<sub>x</sub> or V<sub>1</sub>P<sub>a</sub>M<sub>b</sub>Ti<sub>c</sub>O<sub>x</sub> catalyst wherein M is ~~chosen~~ selected from the group ~~comprising consisting of~~ Cr, Fe, Co and Mo; a is 0.1 - 2.0; b is 0.002 - 1.0; c is 2.0 - 10.0, and x is determined by the valences of other component elements, characterized in that the catalyst contains mainly two phases under working conditions a (VO)<sub>2</sub>P<sub>2</sub>O<sub>7</sub> phase and a (NH<sub>4</sub>)<sub>2</sub>(VO)<sub>3</sub>(P<sub>2</sub>O<sub>7</sub>)<sub>2</sub> phase.

16. (Currently amended) A ~~The~~ catalyst according to claim 15, wherein said carrier is an Al<sub>2</sub>O<sub>3</sub> carrier.

17. (Currently amended) A ~~The~~ catalyst according to claim 15, wherein said carrier is a TiO<sub>2</sub> carrier.

18. (Currently amended) A ~~The~~ catalyst according to claim 17, wherein said TiO<sub>2</sub> carrier consists of the anatase phase.

19. (Currently amended) A method for the preparation of a catalyst according to ~~any of claims 15 to 18~~ claim 15 comprising the steps of:

- preparing a bulk VPO precursor;

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- impregnating said bulk VPO precursor with a promoter element in order to obtain a bulk promoted VPO precursor; and
  - adding a carrier to said bulk promoted VPO precursor,
  - and calcining the resultant mixture under a weakly oxidising atmosphere of O<sub>2</sub>/N<sub>2</sub> to obtain a supported and promoted VPO catalyst.
20. (Currently amended) ~~A-The~~ method according to claim 19 comprising the steps of:
- refluxing of a vanadium source in the presence of alcohols to obtain a solution containing reduced vanadium species;
  - adding of a phosphorus source and refluxing said solution in order to obtain a bulk VPO precursor;
  - impregnation of said bulk VPO precursor with an alcoholic or aqueous solution of a promoter element to obtain a bulk promoted VPO precursor;
  - mixing said bulk promoted VPO precursor with  $\gamma$ -Al<sub>2</sub>O<sub>3</sub> or TiO<sub>2</sub> carrier powder; and shaping and calcining the resultant mixture to obtain a supported and promoted VPO catalyst.
21. (Currently amended) ~~A-The~~ method according to ~~claim 19 or 20~~claim 19, wherein said vanadium source is V<sub>2</sub>O<sub>5</sub> and said phosphorous source is o-H<sub>3</sub>PO<sub>4</sub>.
22. (Currently amended) ~~A-The~~ method according to ~~any of claims 19 to 21~~claim 19, wherein said promoter element comprises Cr, Fe, Co or Mo.
23. (Currently amended) ~~A-The~~ method according to ~~any of claims 19 to 22~~claim 19, wherein the ratio of said bulk promoted VPO precursor over said  $\gamma$ -Al<sub>2</sub>O<sub>3</sub> or TiO<sub>2</sub> carrier powder is ~~comprised~~ in the range of 1:2 to 1:10, ~~preferably 1:6~~.
24. (Currently amended) ~~A-The~~ method according to ~~any of claims 19 to 23~~claim 19, wherein the calcining step is performed at a temperature ~~comprised~~ in the range of 300 to 900°C for a period of 1 to 10 hours, under a calcining atmosphere.
25. (Currently amended) A method according to ~~any of claims 19 to 23~~claim 19, wherein the calcining step is performed at a temperature ~~comprised~~ in the range of 350 to 700°C for a period of 2 to 6 hours, under a calcining atmosphere of weak oxidising strength.
26. (Currently amended) ~~Use of~~A method of using a VPO catalyst obtainable by a process comprising the steps of :
- preparing a bulk VPO precursor ;

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- impregnating said bulk VPO precursor with a promoter element in order to obtain a bulk promoted VPO precursor; and
- adding a carrier to said bulk promoted VPO precursor,
- and calcining the resultant mixture under a weakly oxidising atmosphere of  $O_2/N_2$  to obtain a supported and promoted VPO catalyst,  
whereby said catalyst is a  $V_1P_aM_bAl_cO_x$  or  $V_1P_aM_bTi_cO_x$  catalyst wherein M is selected from the group consisting of Cr, Fe, Co and Mo; a is 0.1 - 2.0; b is 0.002 – 1.0; c is 2.0 - 10.0, and x is determined by the valences of other component elements, characterized in that the catalyst contains mainly two phases under working conditions a  $(VO)_2P_2O_7$  phase and a  $(NH_4)_2(VO)_3(P_2O_7)_2$  phase.

~~according to any of claims 15 to 18~~ and prepared according to ~~any of claims 20 to 26~~ claim 20 in a ~~vapour~~vapor phase ammoxidation reaction.

27. (Currently amended) ~~Use of~~ A method of using a VPO catalyst according to claim 26 ~~in a vapour phase ammoxidation reaction for the preparation of halogenated benzonitriles by vapor phase ammoxidation of halogenated  $C_1$  to  $C_6$  alkyl benzenes, in the presence of water vapor, at a reaction temperature in the range of 300 to 500 °C, using a three-component catalyst into a fixed bed reactor~~ according to any of claims 1 to 15.

28. (Currently amended) ~~Use of~~ A method of using a VPO catalyst according to claim 27 for preparing 2,6-dichlorobenzonitrile from 2,6-dichlorotoluene in a ~~vapour~~vapor phase ammoxidation reaction.

29. (Currently amended) ~~Use of~~ A method of using a VPO catalyst according to claim 28 in a ~~vapour~~vapor phase ammoxidation reaction of hetero aromatic hydrocarbons.

30. (New) The method according to claim 3, wherein the residence time of the halogenated  $C_1$  to  $C_6$  alkyl benzene in said reactor is less than 8 seconds.

31. (New) The method according to claim 23, wherein the ratio of said bulk promoted VPO precursor over said  $\gamma-Al_2O_3$  or  $TiO_2$  carrier powder is in the range of about 1:6.